

## Introduction

*Fluid Power with Applications, 7<sup>th</sup> ed.*, is a great introduction to the field of hydraulics and pneumatics. Most of the equations are algebraic, such as Equation 3-6:

$T = F R$ , where the units of torque  $T$  depend on the units used for force  $F$  and lever arm  $R$ . Some equations include constants that are missing their units. For example, Equation 3-7:  $HP = \frac{TN}{63,000}$ . The units for the constant are  $\frac{\text{hp}}{\text{in.} \cdot \text{lb.} \cdot \text{rpm}}$ , so the equation only works if you enter torque  $T$  in units of in.·lb. and rotational speed  $N$  in units of rpm. This handout lists canned equations used in the textbook and the units for their constants.

## Chapter 3

Eq. 3-5,  $HP = \frac{Fv}{550}$  where power  $HP = \text{hp}$ , force  $F = \text{lb.}$ , velocity  $v = \text{ft./s}$ , and the constant =  $550 \frac{\text{lb.} \cdot \text{ft.}}{\text{hp} \cdot \text{s}}$ .

Eq. 3-7,  $HP = \frac{TN}{63,000}$  where power  $HP = \text{hp}$ , torque  $T = \text{in.} \cdot \text{lb.}$ , rotational speed  $N = \text{rpm}$ , and the constant =  $\frac{63,000 \text{ in.} \cdot \text{lb.} \cdot \text{rpm}}{\text{hp}}$ .

Eq. 3-25,  $HHP = \frac{pQ}{1714}$  where hydraulic horsepower  $HHP = \text{hp}$ , pressure  $p = \text{psi}$ , flow rate  $Q = \text{gpm}$ , and the constant =  $\frac{1714 \text{ psi} \cdot \text{gpm}}{\text{hp}}$ .

Eq. 3-29,  $H_p = \frac{3950 HHP}{Q SG}$  where pump head  $H_p = \text{ft.}$ , hydraulic horsepower  $HHP = \text{hp}$ , flow rate  $Q = \text{gpm}$ , and the constant =  $\frac{3950 \text{ ft.} \cdot \text{gpm}}{\text{hp}}$ .

Eq. 3-37,  $\text{Power} = \frac{T\omega}{1000}$  where power = kW, torque  $T = \text{N} \cdot \text{m}$ , rotational speed  $\omega = \text{rad/s}$ , and the constant =  $\frac{1000 \text{ N} \cdot \text{m}}{\text{kW} \cdot \text{s}}$ .

Eq. 3-37,  $\text{Power} = \frac{TN}{9550}$  where power = kW, torque  $T = \text{N} \cdot \text{m}$ , rotational speed  $N = \text{rpm}$ , and the constant =  $\frac{9550 \text{ N} \cdot \text{m} \cdot \text{rpm}}{\text{kW}}$ .

## Chapter 4

Eq. 4-2,  $N_R = \frac{7740vDSG}{\mu}$  where fluid velocity  $v = \text{ft./s}$ , pipe diameter  $D = \text{in.}$ , absolute viscosity  $\mu = \text{cP}$ , and the constant =  $7740 \frac{\text{cP} \cdot \text{s}}{\text{ft.} \cdot \text{in.}}$ .

Eq. 4-2M,  $N_R = \frac{1000vDSG}{\mu}$  where fluid velocity  $v = \text{m/s}$ , pipe diameter  $D = \text{mm}$ , absolute viscosity  $\mu = \text{cP}$ , and the constant =  $1000 \frac{\text{cP} \cdot \text{s}}{\text{m} \cdot \text{mm}}$ .

Eq. 4-3,  $N_R = \frac{7740vD}{\nu}$  where fluid velocity  $v = \text{ft./s}$ , pipe diameter  $D = \text{in.}$ , kinematic viscosity  $\nu = \text{cP}$ , and the constant =  $7740 \frac{\text{cS} \cdot \text{s}}{\text{ft.} \cdot \text{in.}}$ .

Eq. 4-3M,  $N_R = \frac{1000vD}{\nu}$  where fluid velocity  $v = \text{m/s}$ , pipe diameter  $D = \text{mm}$ , kinematic viscosity  $\nu = \text{cP}$ , and the constant =  $1000 \frac{\text{cS} \cdot \text{s}}{\text{m} \cdot \text{mm}}$ .

## Chapter 5

Eq. 5-2,  $Q_T = \frac{V_D N}{231}$  where pump flow rate  $Q_T = \text{gpm}$ , volumetric displacement  $V = \text{in.}^3/\text{rev.}$ , rotational speed  $N = \text{rpm}$ , and the constant =  $\frac{231 \text{ in.}^3}{\text{gal.}}$ .

**Chapter 6**

Eq. 6-5,  $HP = \frac{vF}{550}$  where cylinder power  $HP = \text{hp}$ , cylinder velocity  $v = \text{ft./s}$ , force  $F = \text{lb.}$ , and the constant =  $\frac{550 \text{ hp}\cdot\text{s}}{\text{ft.}\cdot\text{lb.}}$ .

**Chapter 8**

Eq. 8-1,  $Q = 38.1 C A \sqrt{\frac{\Delta p}{SG}}$  where flow rate  $Q = \text{gpm}$ , orifice area  $A = \text{in.}^2$ , pressure  $p = \text{psi}$ , and the constant =  $\frac{38.1 \text{ gpm}}{\text{in.}^2 \sqrt{\text{psi}}}$ .

Eq. 8-1M,  $Q = 0.0851 C A \sqrt{\frac{\Delta p}{SG}}$  where flow rate  $Q = \text{Lpm}$ , orifice area  $A = \text{mm}^2$ , pressure  $p = \text{kPa}$ , and the constant =  $\frac{0.0851 \text{ Lpm}}{\text{mm}^2 \sqrt{\text{kPa}}}$ .

**Chapter 13**

Eq. 13-8,  $V_R = \frac{14.7 t (Q_T - Q_C)}{p_{max} - p_{min}}$  where receiver size  $V_R = \text{ft.}^3$ , time  $t = \text{min.}$ , flow rate  $Q = \text{scfm}$ , pressure  $p = \text{psi}$ , and the constant = 14.7 psia.

Eq. 13-8M,  $V_R = \frac{101 t (Q_T - Q_C)}{p_{max} - p_{min}}$  where receiver size  $V_R = \text{m}^3$ , time  $t = \text{min.}$ , flow rate  $Q = \text{std. m}^3/\text{min.}$ , pressure  $p = \text{kPa}$ , and the constant = 101 kPa<sub>abs</sub>.

Eq. 13-9, Theoretical power =  $\frac{p_{in} Q}{65.4} \left[ \left( \frac{p_{out}}{p_{in}} \right)^{0.286} - 1 \right]$  where power = hp, pressure  $p = \text{psia}$ , flow rate  $Q = \text{scfm}$ , and the constant =  $\frac{65.4 \text{ psi}\cdot\text{scfm}}{\text{hp}}$ .

Eq. 13-9M, Theoretical power =  $\frac{p_{in} Q}{17.1} \left[ \left( \frac{p_{out}}{p_{in}} \right)^{0.286} - 1 \right]$  where power = kW, pressure  $p = \text{kPa}_{\text{abs}}$ , flow rate  $Q = \text{std. m}^3/\text{min.}$ , and the constant =  $\frac{17.1 \text{ kPa}\cdot\text{m}^3}{\text{kW}\cdot\text{min}}$ .

**Chapter 14**

Eq. 14-3,  $p_f = \frac{0.1025 L Q^2}{3600 C R d^{5.31}}$  where pressure drop  $p_f = \text{psi}$ , pipe length  $L = \text{ft.}$ , flow rate  $Q = \text{scfm}$ , pipe diameter  $d = \text{in.}$ , one constant =  $\frac{0.1025 \text{ in.}^{5.31}}{\text{ft.}^7 \cdot \text{s}^2}$ , and the second constant =  $\frac{3600 \text{ s}^2}{\text{min.}^2}$ .