

Equations and Conversion Factors

Note: the curvy volume symbol in the book is not in a standard font; below, V = velocity and V = volume.

$$\begin{array}{lll}
 W = mg & F_R = P_{avg} A & \text{Pa} = \frac{\text{N}}{\text{m}^2} \\
 A_{circle} = \frac{\pi}{4} d^2 & P = \rho g h & \text{N} = \frac{\text{kg m}}{\text{s}^2} \\
 V_{sphere} = \frac{\pi d^3}{6} & F_B = \rho_{fluid} g V & \text{W} = \frac{\text{N m}}{\text{s}} \\
 \tau = \frac{F}{A} & y_P = y_C + \frac{I_{xx,c}}{\left(y_C + \frac{P_0}{\rho g \sin \theta}\right) A} & \text{J} = \text{N m} \\
 F_{film} = \frac{\mu A V}{l} & \text{Ignoring } P_0: & ^\circ\text{C} + 273 = \text{K} \\
 \Delta P_{droplet} = \frac{2\sigma_s}{R} & y_P = y_C + \frac{I_{xx,c}}{y_C A} & \rho_{water} = 1000 \frac{\text{kg}}{\text{m}^3} \\
 \Delta P_{soap\ bubble} = \frac{4\sigma_s}{R} & \text{Rectangle:} & g = 9.81 \frac{\text{m}}{\text{s}^2} \\
 h = \frac{2\sigma_s}{\rho g R} \cos \phi & I_{xx,c} = \frac{bh^3}{12} & P_0 = 1 \text{ atm} = 101 \text{ kPa} \\
 \\
 \frac{P_1}{\rho g} + \alpha_1 \frac{V_1^2}{2g} + z_1 + h_{pump,u} = \frac{P_2}{\rho g} + \alpha_2 \frac{V_2^2}{2g} + h_{turbine,e} + h_L \\
 P_1 + \alpha_1 \frac{\rho V_1^2}{2} + \rho g z_1 + \rho g h_{pump,u} = P_2 + \alpha_2 \frac{\rho V_2^2}{2} + \rho g h_{turbine,e} + \rho g h_L \\
 h_{pump,u} = \frac{w_{pump,u}}{g} = \frac{\dot{W}_{pump,u}}{\dot{m} g} = \frac{\eta_{pump} \dot{W}_{pump}}{\dot{m} g} \\
 h_{turbine,e} = \frac{w_{turbine,e}}{g} = \frac{\dot{W}_{turbine,e}}{\dot{m} g} = \frac{\dot{W}_{turbine}}{\eta_{turbine} \dot{m} g} \\
 h_L = \frac{e_{mech\ loss, piping}}{g} = \frac{E_{mech\ loss, piping}}{\dot{m} g} \\
 \vec{F}_{thrust} = m \vec{a} = \sum_{in} \beta \dot{m} \vec{V} - \sum_{out} \beta \dot{m} \vec{V} \\
 \dot{m} = \rho V_{avg} A_c & \text{Re} = \frac{V_{avg} D}{\nu} = \frac{\rho V_{avg} D}{\mu} & D_h = \frac{4A_c}{p} \\
 \dot{V} = V_{avg} A_c & h_{L\ pipe} = f \frac{L}{D} \frac{V_{avg}^2}{2g} & h_{L\ fitting} = K_L \frac{V_{avg}^2}{2g} \\
 \text{Laminar: } f = \frac{64}{\text{Re}} & F_L = C_L A \frac{\rho V^2}{2} & \text{Re}_x = \frac{V_{avg} x}{\nu} = \frac{\rho V_{avg} x}{\mu} \\
 F_D = C_D A \frac{\rho V^2}{2} & &
 \end{array}$$

Inside a round pipe: laminar if $Re < 2300$, transition if $2300 < Re < 4000$, turbulent if $4000 < Re$

Over a sphere or cylinder: laminar if $Re < 2 \times 10^5$, transition if $2 \times 10^5 < Re < 2 \times 10^6$, turbulent if $2 \times 10^6 < Re$

Over a flat plate: laminar if $Re < 5 \times 10^5$, then average $C_f = \frac{1.33}{Re_L^{1/2}}$

Over a flat plate: turbulent if $5 \times 10^5 < Re$, then average $C_f = \frac{0.074}{Re_L^{1/5}}$

Flat plate with both laminar & turbulent boundary layers: $C_f = \frac{0.074}{Re_L^{1/5}} - \frac{1742}{Re_L}$

Aircraft $V_{min} = \sqrt{\frac{2W}{\rho C_{L,max} A}}$

Metric prefixes

n	=	nano-	=	10^{-9}	k	=	kilo-	=	10^3
μ	=	micro-	=	10^{-6}	M	=	mega-	=	10^6
m	=	milli-	=	10^{-3}	G	=	giga-	=	10^9
c	=	centi-	=	10^{-2}	T	=	tera-	=	10^{12}